

# Design of a Process for Direct Air Capture in Nova Scotia

## Project Background

Increased industrial activities and the combustion of fossil fuels has led to the high concentrations of carbon dioxide (CO<sub>2</sub>) found in the atmosphere. CO<sub>2</sub> emissions are considered a leading contributor to climate change. To help mitigate the harmful impacts of CO<sub>2</sub> emissions, direct air capture (DAC) technology has been identified as the most efficient method of permanently removing CO<sub>2</sub> from the atmosphere.



The purpose of this project was to design a process for DAC located in the Province of Nova Scotia and assess the feasibility through an economic and safety/sustainability analysis.

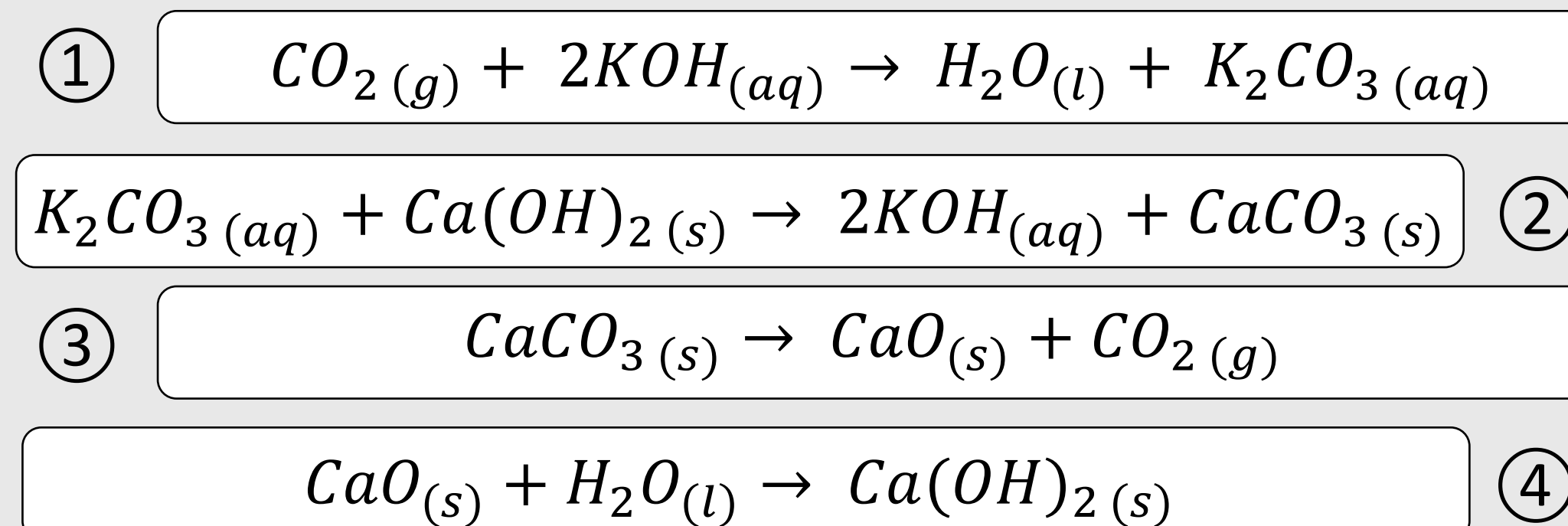
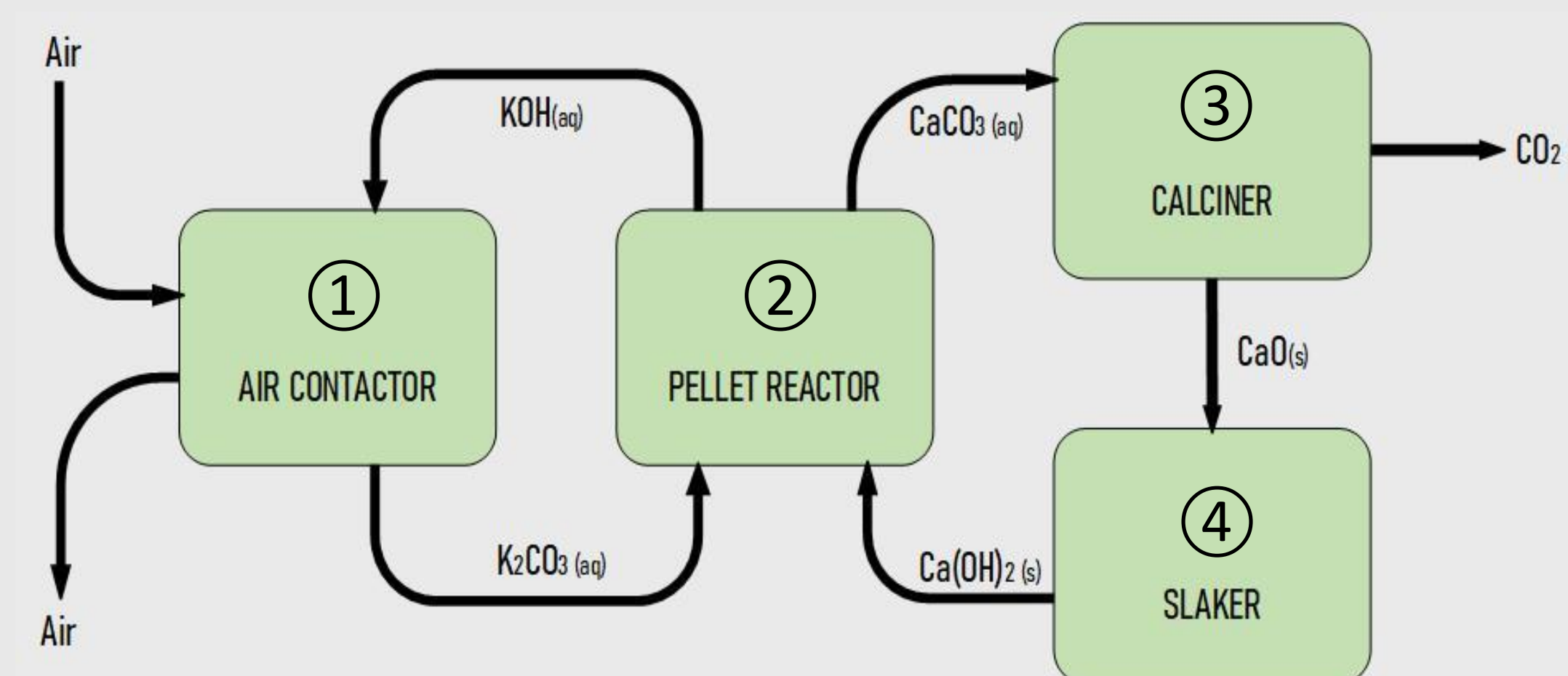
## Design Objectives

The following are key objectives for the proposed design:

- The plant must be located within Nova Scotia
- The process should allow for continuous operation, running for 8000 hours/year
- The CO<sub>2</sub> product stream should have a purity of at least 95%
- The process must result in negative emissions

## Process Overview

After conducting an in-depth literature review, the chosen approach consisted of the use of KOH as the solvent and a quick lime cycle. The process is as follows:



## Details of Design

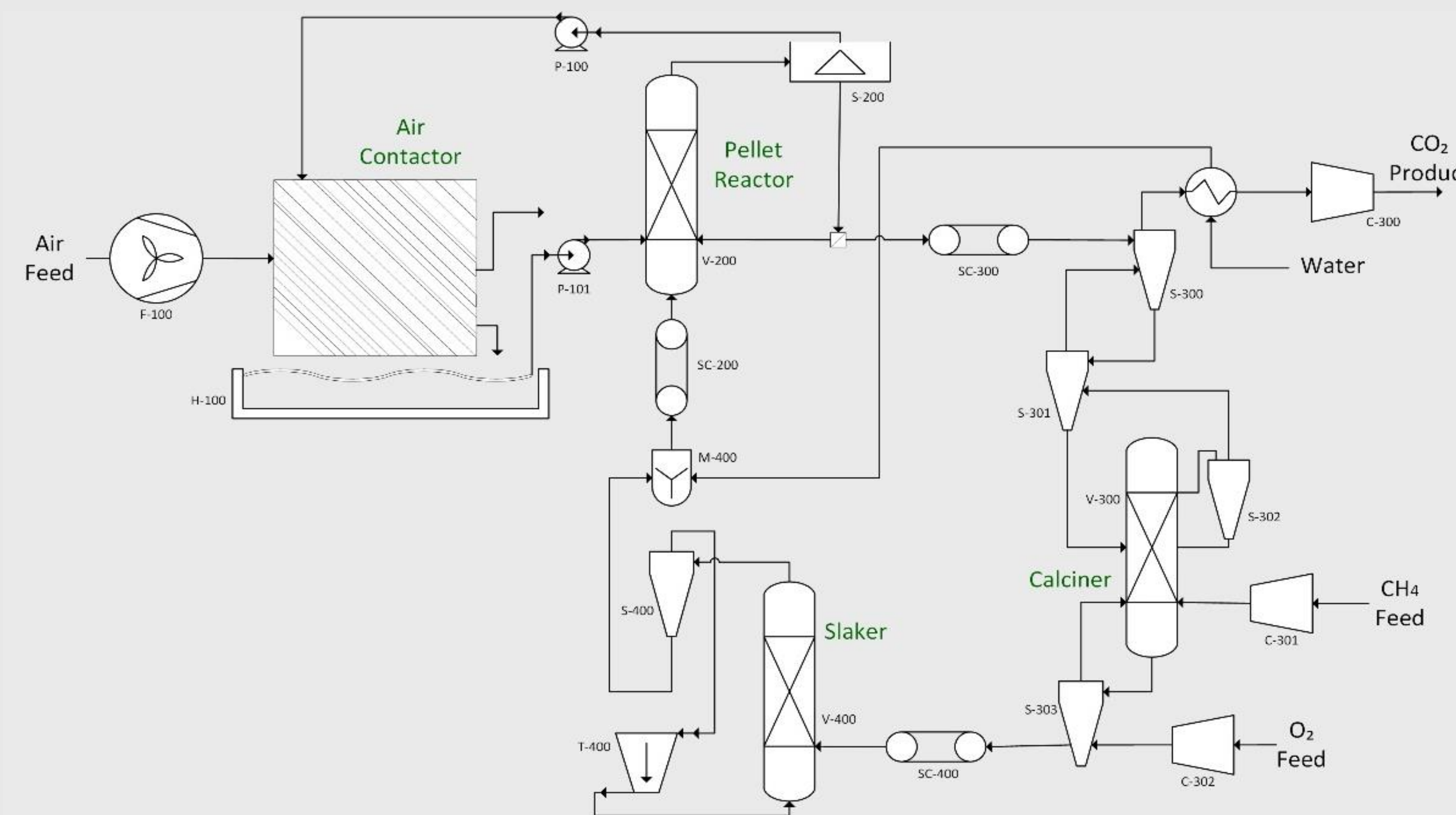


Figure 1 – Process flow diagram for the preliminary design of the proposed DAC process

### AIR CONTACTOR

The air contactor contains a large fan that pulls air into a packing that selectively reacts CO<sub>2</sub> with the flowing KOH. The air contactor has a CO<sub>2</sub> conversion of 91.4% to form K<sub>2</sub>CO<sub>3</sub> that is fed into the pellet reactor.

### PELLET REACTOR

The pellet reactor process consists of a circulating fluidized bed reactor and a sedimentation centrifuge. A slurry of 30 wt% Ca(OH)<sub>2</sub> from the slaker and aqueous K<sub>2</sub>CO<sub>3</sub> solution from the air contactor are fed into the bed. These components undergo the exothermic reaction with a conversion rate of 90% to generate CaCO<sub>3</sub> particles no larger than 588 μm in diameter. The particles are heated to 300°C before being sent to the calciner.

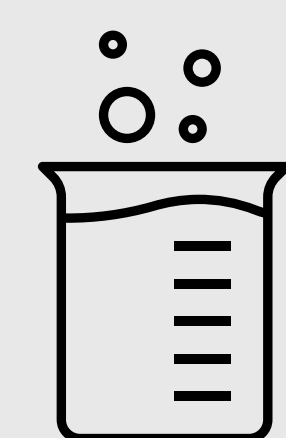
### CALCINER

The calciner is an oxygen-fired circulating fluidized bed reactor that plays a critical role in the regeneration of the captured CO<sub>2</sub> from CaCO<sub>3</sub>. Methane is fed at a flow rate of 1.6 kg/s to maintain the reactor temperature of 900°C such that 98% CO<sub>2</sub> is regenerated.

### SLAKER

The slaker is composed of a bubbling fluidized bed reactor, where the CaO hydration reaction is carried out at a temperature of 350°C. The reaction is carried out with a conversion rate of 85%, with the resulting Ca(OH)<sub>2</sub> mixed into slurry before being recycled back to the pellet reactor for regeneration.

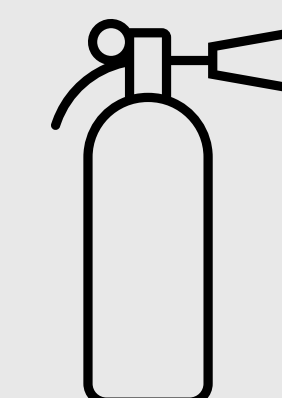
## Safety Considerations



Runaway reactions



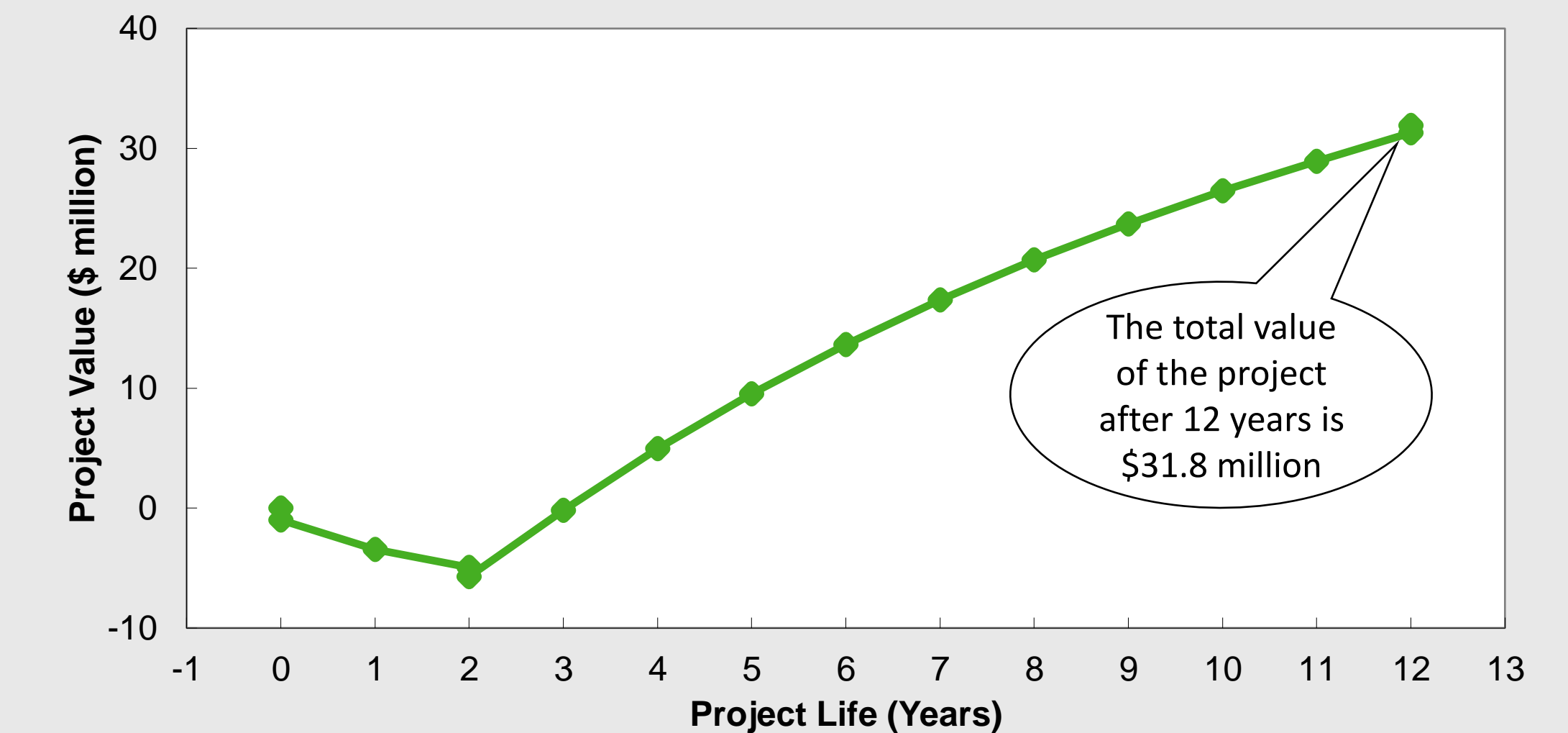
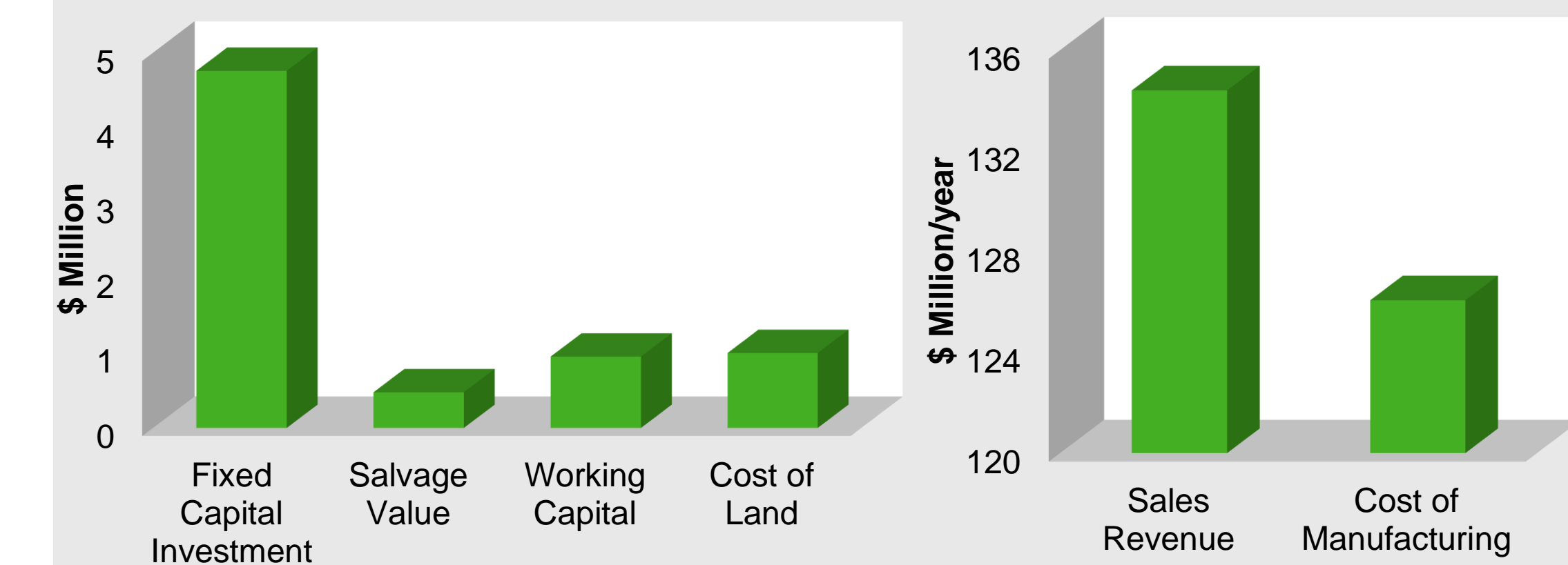
Dust formation & airborne debris



Overpressurized systems

## Energy-Use and Economics

- The process requires **1061 kW** of electricity
- 5.3 tonnes** of CO<sub>2</sub> is captured through the air contactor per hour
- 26 tonnes** of CH<sub>4</sub> is required for thermal energy per hour, making up more than **99%** of the energy requirements
- 100%** of CO<sub>2</sub> formed from combustion is captured
- For every **1 gram** of CO<sub>2</sub> emitted from the process, **217 grams** are captured



## Conclusion & Recommendations

- The process produces 97.5% CO<sub>2</sub> at 13.4 ton/hr.
- The process results in a net value of \$31.8 million
- The process is carbon negative

### Recommendations

- Future work use renewable energy
- Future study on noise pollution

## References

Keith, D. W., Holmes, G., St. Angelo, D., & Heidel, K. (2018). A Process for Capturing CO<sub>2</sub> from the Atmosphere. *Joule*, 2(8), 1573–1594. <https://doi.org/10.1016/j.joule.2018.05.006>

Kunii, D., & Levenspiel, O. (1991). *Fluidization Engineering* (2nd Edition). Butterworth-Heinemann.